

1 **Particle and liquid motion in semi-solid aluminium alloys:**  
2 **a quantitative in situ micro-radioscopy study**

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11 **Abstract**

12 Semi-solid melt exhibits a very unpredictable rheology and filling dynamics, when it is injected  
13 into thin-walled components. Optimization of the process requires visual insight into the  
14 casting process during the injection. For this purpose we inject semi-solid Al-Ge alloy into two  
15 different thin channel geometries while recording high-resolution radiographs at fast frame  
16 rates (up to 1000 images/s). The comparison of a bottleneck channel, which had been  
17 previously used for slower experiments, with a right-angle turn geometry reveals a significant  
18 influence of the channel's shape on the flow behavior of the particle-liquid mixture. While the  
19 bottleneck is quickly sealed with densified solid, turbulences in the right-angle turn apparently  
20 permit the solid particles and clusters to move conjointly with the liquid and thus achieve a  
21 more complete filling. Single particle trajectories and rapid break-up of solid skeletons in such a  
22 system are observed for the first time in situ.

23 **Keywords:** Semi-solid, X-ray radiography, synchrotron radiation, rheology, in-situ.

24 **1. Introduction**

25 Semi-solid metals are two-phase solid-liquid mixtures of unusual rheological properties  
26 [1]. While they are inert, they behave like elastic solids, whereas shearing causes a transition  
27 into a viscous mixture which can flow. Thus, they show shear thinning behaviour, i.e. the  
28 apparent viscosity drops exponentially when the shear rate is increased. The transition from a  
29 sponge-like locked solid phase filled by liquid to a viscous medium is marked by the breakup of  
30 the (percolated) solid skeleton into particles and/or clusters which can move individually  
31 through the liquid. This breakup is commonly referred to as the '*thixotropic effect*' [2]. Typical

1 alloys which are used for thixo- or rheocast components are aluminium and magnesium  
2 casting alloys (e.g. A356 or AZ91). Compared to high pressure die casting, semi-solid casting  
3 (SSC) processes operate at lower temperature which is associated with a number of  
4 advantages [3], namely that volume shrinkage effects are less pronounced, there is far less risk  
5 of hot cracking and void formation and die wear is reduced due to the low temperatures. The  
6 compositional range of casting alloys can be extended to larger melting intervals. On the other  
7 side, various difficulties lead to higher costs and have so far prevented the technology from  
8 becoming wide spread.

9 While the flow of the liquid phase can be described as a Newtonian fluid, little is known  
10 about the flow and rheology of a solid-liquid mixture [4]. The size and shape of solid particles /  
11 clusters, their motion, their ability and tendency to break up and regroup into different  
12 morphologies are a critical input required to model the filling dynamics of semi-solid injections  
13 [5]. There are many possible interactions: particle-particle as well as particle-liquid: e.g.,  
14 diffusion, van-der-Waals forces, adhesion, particle-particle necks and electrostatic interactions.  
15 Commonly, semi-solid rheology is measured in terms of the apparent and / or complex  
16 viscosity  $\eta$  in experimental rheometers (either rotating bob or oscillating plate geometry).  
17 These measurements require a very sophisticated and costly setup since they have to cover  
18 some 8-10 orders of magnitude of viscosity. Systematic dependencies of  $\eta$  on temperature,  
19 hence on solid fraction, shear rate and time have been well studied [6]. These observations are  
20 however not visual and, hence, insufficient to fully describe and predict the die casting process.  
21 The quality of the latter can only be judged ex-situ from the cast components (e.g. spiral or  
22 other testing moulds), whereby the die filling properties of SSC are known to be rather poor for  
23 the casting of thin components. This drawback is not only due to the higher viscosity of the  
24 mixture as compared to the liquid, but also to demixing which is taking place during SSC.  
25 Thereby, the furthest extremities of the mould, particularly in thin geometries, fill mostly with  
26 liquid, while the solid fraction of the core is raised artificially. Consequently, microstructure and  
27 mechanical properties of the components become inhomogeneous. For binary or quasi-binary  
28 alloys this demixing can further lead to reduced fatigue strength because the liquid phase with  
29 its higher concentration of alloying elements has a more brittle microstructure. In order to learn  
30 more about this demixing of solid and liquid, the die filling process has to be observed in situ.

31 The authors have recently presented first results on an in situ visualization of semi-solid  
32 Al-Ge alloy injected through a thin cavity and recorded by synchrotron X-ray radioscopy [7]. Yet,

1 the employed acquisition rate of 66 images/s and below showed to be at least an order of  
2 magnitude too slow to follow the real injection process, whereas this rate was found to be well  
3 suited to study granular deformation mechanisms in semi-solid alloys under shear [8, 9, 10].  
4 For this work, the previously described experiment could be extended to a rate of 500  
5 images/s by moving to the high energy beamline ID15a of the European Synchrotron  
6 Radiation Facility (ESRF), Grenoble, France. ID15a has a photon flux density which is sufficient  
7 to record high-resolution radiographs at this high rate [11, 12]. Also the in situ setup has been  
8 developed further, in terms of temperature control and injection speed. For the present work  
9 we used two different thin channels to compare for the injection of an Al-Ge32 alloy: a) a  
10 bottleneck (similar to our previous study [7]), b) a right-angle turn channel. Optical flow  
11 analysis was then applied to track and to quantify particle and liquid motion in the measured  
12 data. This work demonstrates the unique capabilities of third generation synchrotron light  
13 sources to visualize microscopic deformation of semi-solid metals in situ.

## 14 **2. Materials and methods**

### 15 *2.1. Semi-solid injection process*

16 Figure 1 shows two photographs of the experimental setup which consists of an in situ  
17 furnace with a linear motor driving injection, and an imaging system. The furnace is an  
18 aluminium case fully covered with vermiculite plates in order to shield the heat which is  
19 produced by four Osram Xenophot 64635 HLX heating lamps (150 Watts, 15 Volts) which are  
20 slightly defocused and point towards the sample holder. The holder is a sandwich of two  
21 structured boron nitride (BN) plates which are held together by an alumina frame, as discussed  
22 in Zabler et al. 2010 [7]. A 0.5-mm thin thermocouple (Ni-Cr(+)/Ni-Al(-) type K, Thermocoax  
23 SAS, France) protrudes into the BN sandwich right next to the piston, just 1 mm to the right of  
24 the flow channel. The X-ray pencil beam enters and leaves through two holes in the front and  
25 back of the vermiculite plates and only passes through the BN structure. A 0.4-mm sheet of  
26 stainless steel (304 L) is attached to a linear stepping motor (Phytron, Inc., USA) and serves as  
27 a piston, driving downwards into the sandwich structure at 20 mm/s maximum velocity,  
28 thereby injecting the semi-solid material into the channel. The alloy Al-Ge32(wt.%) was chosen  
29 for being very similar to commercial Al-Si7 alloys concerning microstructure, yet having a  
30 larger X-ray density contrast between liquid and solid phase. The temperature for the SSC  
31 process is lower than in AlSi7, given by the solidus temperature of  $\sim 420^{\circ}\text{C}$  and liquidus  
32 temperature of  $\sim 550^{\circ}\text{C}$ ). Small platelets of 7 mm x 3 mm x 0.4 mm were cut from as-cast ingots

1 to which 4 wt.% Al-Ti5-B grain refiner (Affilips Netherlands) were added to obtain a fine  
2 equiaxed microstructure. Prior to the experiments, all samples were heat-treated for 1 h in the  
3 semi-solid state at 480°C to produce coarse globular particles of about 50 µm average diameter.

4 Before starting the experiment, the effect of sample heating through irradiation by the X-  
5 ray beam was tested by placing a 4-mm thick piece of Al-Ge32 alloy in our setup with the lamps  
6 being turned off. The sample had a hole into which the thermocouple was placed and measured  
7 a temperature increase of 6 K while the X-rays were impinging onto the metal. Since the photon  
8 absorption of the 0.4-mm thick sample used for the radioscopy experiment was at least an  
9 order of magnitude smaller it is safe to assume that the heating by radiation was a few K at  
10 most. The two experiments, each with a different channel geometry, both took place at T =  
11 520°C temperature. To exclude the possibility of a measurement error due to the thermocouple  
12 (shielded by an Al<sub>2</sub>O<sub>3</sub> tube) which might be heated by the IR heating lamps or by scattered X-  
13 radiation, metallographic sections were recorded of the cold alloy microstructure after the  
14 radioscopy experiment. The velocity of the piston was set to 20 mm/s, the maximum  
15 acceleration being 80 mm/s<sup>2</sup>. The amplitude of the movement was set to 8 mm, but the motion  
16 stopped earlier during both runs, i.e., when the solid skeleton had densified sufficiently  
17 through compression at the entrance of the BN-channel. After each experiment the samples  
18 were cooled down in air, extracted from the BN-sandwich and passed on for metallographic  
19 investigation under the light microscope.

## 20 2.2. *Synchrotron-based microradioscopy*

21 By employing hard polychromatic X-ray synchrotron radiation, radioscopy was  
22 successfully performed with acquisition rates ranging from a few hundred up to several ten  
23 thousand images per second [13, 14]. While X-ray inline phase contrast can frequently be  
24 employed in order to allow for high acquisition rates, our experiment required sufficient  
25 absorption contrast in order to separate qualitatively and quantitatively the liquid and the solid  
26 phase in the projection images. Hence, the high flux and high energy beamline ID15a (ESRF)  
27 was chosen to carry out this study: An outstanding high photon flux density is available, while  
28 the demands on coherence are less stringent. The employed insertion device of the beamline is  
29 an asymmetric multipole wiggler (1.84 T, 44 keV critical energy, further details available online  
30 [15]). ID15a was operated in a so-called 'white beam mode': the radiation from the source was  
31 filtered only by approximately 20 mm of silicon resulting in a photon flux density of approx.  
32 10<sup>15</sup> ph/mm/s. The X-ray image detector was an indirect system, designed and constructed by

1 the ESRF detector group [16]: A commercial tele-lens projects the luminescence image of a  
2 scintillator screen via a mirror (periscope geometry) onto the sensor of a CMOS camera. The  
3 mirror is used in order to prevent direct exposure of the camera electronics to the intense  
4 synchrotron radiation. As luminescence screen, a 100- $\mu\text{m}$  thick YAG:Ce (Ce-doped  $\text{Y}_3\text{Al}_5\text{O}_{12}$ )  
5 single crystal was chosen. This material is known to resist the high heat load of the white beam  
6 from a synchrotron light source as well as for its fast response time[11]. In order to acquire  
7 images with high frame rates, a Photron SA1 camera was used, which is based on a CMOS  
8 sensor with  $1024 \times 1024$  pixels, each 20  $\mu\text{m}$  in size and a true dynamic range of 800:1 grey  
9 levels (10 bit, with a 12 bit digitalization). The camera can acquire up to 5400 images/s in full-  
10 frame mode. A memory of 32 GB on board allows for the intermediate storage of the images  
11 acquired and hence defines the maximal length of the recordable high-speed movie. Due to the  
12 optical magnification, the complete detector operates with an effective pixel sampling of  
13 5.5  $\mu\text{m}$  (hence, the spatial resolution is  $R > 11 \mu\text{m}$ , according to the Shannon theorem). For this  
14 study the acquisition rate was 500 images/s ('bottleneck' movies) and 1000 images/s ('right-  
15 angle turn' movies). As the readout time of the CMOS sensor is in the  $\mu\text{s}$  range, each picture  
16 corresponds to an exposure of 2 ms or 1 ms, respectively. The detector was positioned as close  
17 as possible to the sample (approximately 0.1 m distance) in order to reduce X-ray inline phase  
18 contrast effects.

### 19 2.3. *Image processing and optical flow analysis*

20 For the task of particle and liquid flow analysis we used automated optical flow techniques  
21 which are built to find correspondences between successive frames. This technique relies on  
22 the formulation of a variational problem, and determines a displacement field as its solution  
23 [17]. The original raw data comprises a number of difficulties, such as low signal to noise ratio,  
24 low contrast between particles and bubbles and temporally non-uniform brightness flickering.  
25 Such problems have occurred in other optical flow computations of X-ray microradiography  
26 [18]. Since optical flow methods are very demanding on image quality, it was crucial to  
27 augment the original radiographs quality prior to optical flow computations. An advanced pre-  
28 processing routine was therefore derived to improve the raw data and meanwhile preserve  
29 spatial and temporal details. The routine starts by applying a 3D Hybrid median filter [19] to  
30 eliminate the high contrast speckle noise. In order to equalize the non-uniform brightness  
31 variations, we then apply a spatial high-pass filter. This part of the process removes large-scale  
32 brightness patterns and retains local details. Finally, we used an anisotropic diffusion filtering

1 to eliminate the image noise and at the same time to enhance particle edges. The entire image  
2 pre-processing was performed with the freely available ImageJ software [20].

3 In order to compute reliable flow fields we employed an advanced optical flow model, which  
4 takes into account multiple image features and a priori motion information. For the  
5 construction of the model we assume constancy of image brightness and of spatial intensity  
6 gradients [21]. This combined assumption is more suitable for the motion estimation, if the  
7 image features are of low contrast. To provide robustness against noise, the data constancy  
8 assumptions were extended by a combined local-global approach [22]. For the motion  
9 constraint we chose a flow-driven smoothness approach [21]. The rather high image  
10 acquisition rate (500 images/s) resulted in a smooth gradual motion of the constituents, from  
11 which we can benefit by introducing an additional spatio-temporal smoothness constraint  
12 [21]: i.e., the final model takes into account motion between more than two successive frames.  
13 Furthermore, to separate the motion of the liquid front from the flow of adjacent particles, the  
14 smoothness is adapted to a spatial mask covering the air-liquid interface (cf. Fig. 2). In order to  
15 cope with a large range of flow velocities a coarse-to-fine computation strategy [21] has been  
16 incorporated. The result of the optical flow computation is a displacement vector for each  
17 image pixel. In order to visualize the latter we use a colour wheel, which indicates the direction  
18 by colour and the velocity by brightness.

### 19 **3. Results**

20 Figure 2 shows three versions of a radiographic image (frame #140) taken from the  
21 bottleneck sequence [Movie1 download]: (a) the normalized raw data, (b) data after filtering,  
22 masking and noise reduction and (c) the calculated colour-coded flow field. Noise reduction  
23 through filtering was essential to provide sufficient quality for the flow analysis. One can clearly  
24 distinguish between liquid and solid phase whereby the latter appears darker due to the lower  
25 X-ray density of aluminium compared to the Ge-rich liquid matrix. Air bubbles are difficult to  
26 distinguish from the Al particles. Compared to the latter, they descend at higher velocities and  
27 appear darker in the radiographs (arrow 1 in Fig. 2b). Two or three small clusters of solid  
28 particles detached from the bulk and moved through the channel following the liquid-air  
29 interface (arrow 2 in Fig. 2b). Their velocity signal overlaps with the signal of the liquid-air  
30 interface. This overlap depends on a 'smoothness constraint' of the optical flow analysis, which  
31 is a compromise between flow continuity and flow detail. One isolated particle appears not to  
32 move at all in this frame (arrow 3), whereas the expanding liquid forms a semi-circular crest of

1 constant velocity (as expected for a Newtonian fluid). The movement of the solid bulk in the  
2 upper part of the radiograph is slow and thus can hardly be observed in Fig. 2c (arrow 4).

3 For the same frame which is shown in Fig. 2 the quantitative flow amplitude (without  
4 direction) is calculated and shown in Fig. 3. The liquid is found to advance at a maximum speed  
5 of 3.1 mm/s, with the air bubbles descending at relatively high speed, up to 3.9 mm/s. The  
6 speed of the particle cluster at the lower liquid-air interface is 1.6 mm/s, and the average speed  
7 of the solid bulk in the upper part of Fig. 3 remains  $< 0.3$  mm/s. A projected time evolution of  
8 these elements is shown in Fig. 4. Here, the average velocity was projected for each pixel over  
9 several hundred frames, i.e. integrating from frame #50 to frame #250, while removing the  
10 velocities of the liquid front with a 3D contour mask [Movie2 download]. The resulting colour-  
11 coded velocity projection (Fig. 4a) shows solid particles, clusters and air bubbles. The latter  
12 follow a curved trajectory until the downwards directed pressure is balanced by the buoyant  
13 force and their motion describes a hook. The few particles, whose velocities overlap with the  
14 crest of the liquid front (cf. Fig. 2), are seen in the lower right. Quantitative velocity amplitudes  
15 are shown in Fig. 4b, which allow to draw velocity-path profiles (along the curved arrows), for  
16 air bubbles (path 1), and for particle clusters (path 2). The profiles are shown in Fig. 5 where  
17 the velocities of the air bubbles appear significantly faster (slightly slower than the liquid)  
18 compared to the particle cluster: 3 – 4 mm/s (before the bubble slows down and its velocity  
19 approaches 1 mm/s), compared to 0.5 – 1.0 mm/s for the cluster, respectively.

20 To investigate the flow of the solid skeleton over the remaining time sequence, average  
21 velocities were integrated from frame #250 to #450. The radiographs were again 3D-masked  
22 to separate liquid and solid. Figure 6 shows the average velocities for both components.  
23 Velocity of the solid particles appears to be of homogeneous amplitude, yet differing in  
24 direction, resulting in a faceted structure (cf. Fig. 6a). The integrated velocities in Fig. 6a also  
25 match with the silhouette of the final state of the solid skeleton reaching into the recipient  
26 (which was not fully filled by solid) and matches metallographic post-observations. On the  
27 other hand, the projected liquid flow appears smooth and homogeneously distributed, filling  
28 the entire cavity (cf. Fig. 6b). As expected from Bernoulli's law on fluids, the liquid velocity in  
29 the recipient (3 mm x 0.4 mm) equals 1/3 of the value which is measured in the narrower  
30 bottleneck (1 mm x 0.4 mm).

31 Figure 7a shows the last radiography of the sequence, Fig. 7b the corresponding  
32 metallographic section which was prepared after the experiment. The microstructure shows

1 portions of the alloy which were fully liquid at the end of the experiment and hence secondary  
2 Al-dendrites formed during cooling. The volume fraction of these dendrites is calculated from  
3 the metallographic sections and marks a fixed point on the liquidus line in the binary phase  
4 diagram, hence the temperature during the experiment. The 35-40 vol.% which are found are  
5 in good agreement with the measured 520 °C which corresponds to a value of 38 vol. % for the  
6 secondary dendrites. Hence, the solid fraction at 520 °C is 22 vol.% according to the binary  
7 phase diagram.

8       When the experiment is carried out with a different channel geometry (right-angle turn)  
9 the flow behaviour is expected to change [Movie3 download]. The right-angle was chosen to  
10 create a more turbulent flow, in the hope that the motion of both liquid and solid would be  
11 more conjoint compared to the bottleneck. Figure 8 shows a series of three radiographs  
12 situated in the middle of the sequence (a-c) covering about 0.2 s, and the metallographic  
13 section of the final structure (d). The solid phase appears indeed to stay closer to the liquid  
14 front, larger round air bubbles move along and disappear at some point of time. Projection  
15 maps of average velocity (directional, i.e. colour-coded) of the solid phase are shown in Fig. 9  
16 for the right-angle geometry, along with an attempt to divide the channel into three distinct  
17 regions: I, II and III. Fig. 9 results from integration over the first half of the sequence, hence  
18 frame #100 to #450. The colour-coding clearly shows that in region I the solid phase moves in  
19 curved trajectories through the channel following the right-angle turn (cf. Fig. 9a). Yet, in the  
20 lower part of the channel (region II) hardly any movement takes place. The motion in region III  
21 is directed downwards and reveals slow particle motion as well as some larger bubbles  
22 descending faster (cf. Fig. 9b). Numerous particles which exhibit momentarily some turbulent  
23 motion appear as bright coloured speckles. Some of these speckles correspond to air bubbles  
24 like the ones observed in Fig. 4a, but some are actually particles whose velocities remind of a  
25 Brownian-like motion. An example for this motion can be seen in Fig. 10. During a series of 23  
26 frames the particle appears to detach from a large cluster and moves in various directions  
27 before re-joining the solid skeleton. An example of spontaneous break-up of a larger particle  
28 cluster from the latter is displayed in Fig. 11. A large region of the solid, approx. 1.5 mm in  
29 diameter which is located at the interface between region I and II, remains frozen for approx.  
30 35 ms (Fig. 11a), then suddenly the upper half of this cluster moves at high speed into separate  
31 directions, indicated by several flares in Fig. 11c (velocity amplitude), while the lower part  
32 remains still.



#### 4. Discussion

Compared to our previous experiments [7] the present data shows a multitude of dynamic effects, particularly for the new geometry (right angle turn) of the flow channel. Here, isolated turbulent particle motion and transition from a frozen solid skeleton to moving particle / clusters could be observed. The latter, we believe, is the first visual proof of the thixotropic break-up during semi-solid injection. Concerning the bottleneck channel our results match previous observations of slower injections [7], despite being an order of magnitude faster than the latter. When the channel narrows, only few particles traverse the bottleneck, the remains accumulate at the entrance. The solid movement comes to a complete halt, when the liquid has fully filled the recipient, balancing the top-down pressure from the piston or when the compressed solid particles block further flow through the channel. Compared to the slower experiments, we used a higher temperature and hence a smaller solid fraction (22 vol% instead of 48 vol%), as well as a faster piston (20 mm/s instead of 2 mm/s). The transport of particle clusters through the bottleneck appears to be hindered mainly by inter-particulate friction (with the exception of a few particle clusters moving directly on the crest of the liquid-air interface). This can be explained by the particle clusters moving independently, often not along a straight line and with possible rotations and mutual collisions. Our results show clearly the inter-particulate as well as the particle-wall friction to be the hindering force during semi-solid injections through thin cavities.

Concerning the data interpretation we have adapted algorithms by means of optical flow analysis for the tracking of in situ rheological motion of semi-solid melt by introducing and adjusting a variety of numerical constrains (such as smoothness, flow-driven approach) based on different assumptions (e.g. constancy of total brightness and of gradients). Compared to the raw data which was prone to brightness artefacts and strong image noise, the resulting flow charts are impressively clear. Our computation is not limited to the present problem, many other applications exist: e.g., motion of granular material and high-speed X-ray movies of laser welding, where ceramic particles serve as contrast agent to visualize the flow of the melt. Our experiments are the first to visualize semi-solid metal flow at such high speed (500 images/s and 1000 images/s, i.e. 2 ms and 1ms sampling of the time domain, respectively). By applying optical flow analysis, velocities up to 5 mm/s were measured for the liquid, 3.6 mm/s for the solid phase. Note, that the piston which accelerated downwards, reaching 20 mm/s maximum speed was much faster than the liquid. Yet, the latter was also sucked up through the gap

1 between BN walls and the downwards driving piston, thus reducing the pressure, which  
2 explains the somewhat low velocities measured with this experimental setup. Recording even  
3 faster scenes on the same beamline (ID15a) is unlikely to provide more details, since the signal-  
4 to-noise ratio (SNR) of the present movies shows the very limit required by the flow analysis.  
5 On the other hand, using the polychromatic spectrum of a beamline with softer X-emission  
6 (e.g. 20-50 keV) could raise the absorption contrast (which in this study was  $\mu t = 0.45$ , with  $\mu$   
7 being the attenuation coefficient and  $t$  the effective thickness of the sample along the X-ray  
8 beam path) and thus the SNR. Recently, on the ID19, radioscopic movies of metal foaming were  
9 recorded at a rate as high as 105 000 images/s using a wiggler source in 'white-beam mode'  
10 [23, 24].

## 11 **5. Conclusions**

12 The comparison of the semi-solid flow through two types of thin channel geometries  
13 indicates a significant influence of the latter on the filling properties of semi-solid metals.  
14 During injection into the bottleneck channel, only little solid material could descend through the  
15 channel into the cavity, which was hence mainly filled with liquid. On the contrary, both solid  
16 and liquid phase moved relatively conjointly through the right-angle turn in the second  
17 experiment, which was found to locally exhibit turbulent flow resulting in Brownian-like  
18 particle motion and breakup of larger clusters into smaller particles. Events showing the  
19 appearance and disappearance of gas bubbles were more frequently observed in the right-  
20 angle turn. It appears that the less laminar flow of the liquid which takes place in such channel-  
21 turns and -corners allows the solid skeleton to advance at a similar speed with the liquid. The  
22 problem of the bottleneck is that the slow network of solid particles at the top entry into the  
23 channel is all too quickly depleted from liquid phase which is needed by the particles to move.  
24 Since the overall amount of liquid is limited by the composition of the alloy, it is only at the  
25 very beginning of the experiment that solid particles are crossing the channel. An interesting  
26 variation of this experiment would be to put a larger piece of Al-Ge alloy (with a Ge-  
27 concentration high enough to fully melt the piece) on top of the semi-solid Al-Ge32, thus  
28 providing a continuous flow of liquid during the injection. One unexpected conclusion of this  
29 study is that during the semi-solid injection, the diffusion and dissolution of the constituting  
30 elements is slow compared to the motion of solid and liquid phase. One could therefore easily  
31 use more liquid without dissolving the solid phase.

32 The next logical step would be to vary the temperature during the experiment thus

1 changing the solid volume fraction of the mixture. Yet, the present results show that already a  
2 fraction as low as 22% has problems penetrating the bottleneck. Another step ahead would be  
3 to compare the radioscopic observation with 3D finite element studies of the semi-solid flow.  
4 The impact of particle size and shape could thus be tested.

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